

Deep Eutectic Solvents

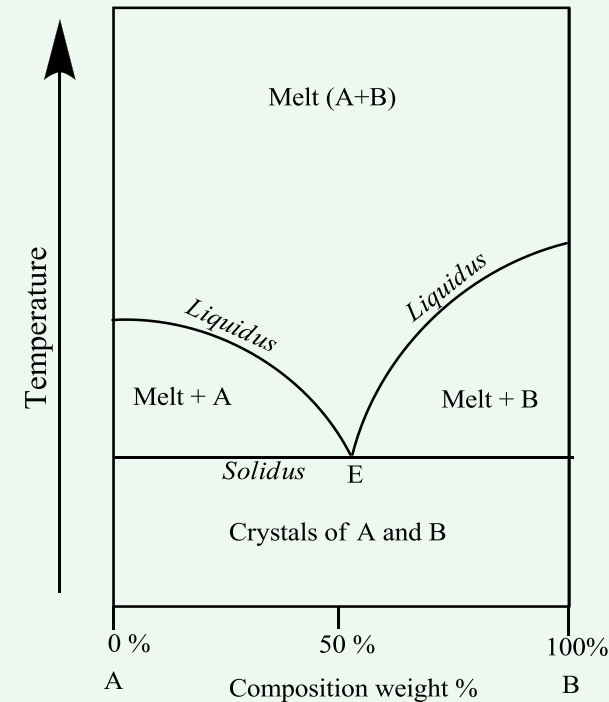
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Contents

- Definitions
- Physical Properties
- Applications – synthesis, electrochemistry, metal processing

Eutectics

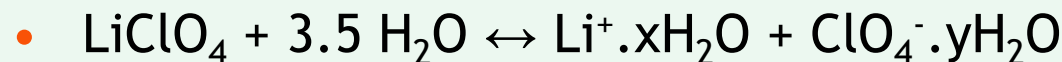
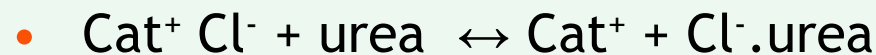
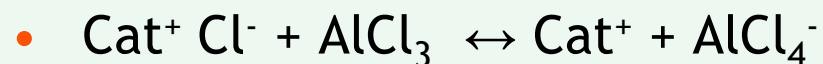
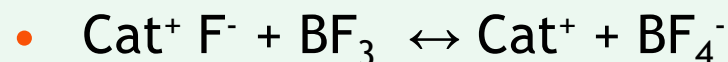
- Mixture of 2 compounds that has the lowest melting point (E)
- Depression of freezing point related to the strength of interaction between the two components



First vs. Second generation ILs

- cation + anion + complexing agent \leftrightarrow cation + complex anion
or potentially

- cation + anion + complexing agent \leftrightarrow complex cation + anion



All that changes is the value of the equilibrium constant

Key Requirements for a New Solvent

- Low cost
- High solute solubility
- Wide potential window
- Environmental compatibility
- No registration requirements

To satisfy these criteria it is necessary to use eutectic based ionic liquids

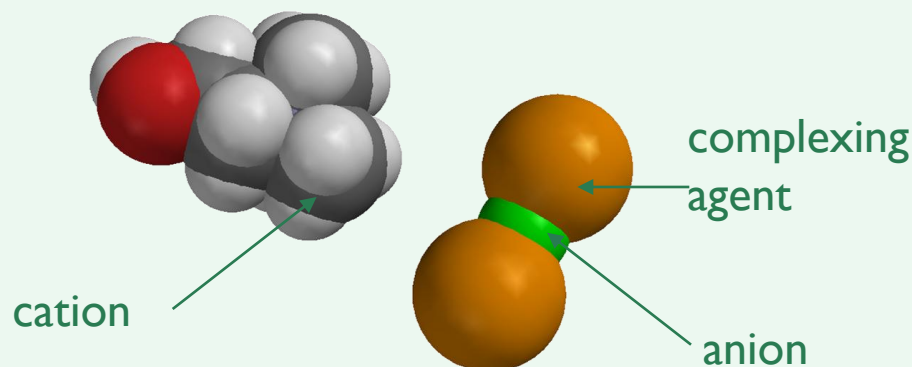
Why choline chloride?

- Non-toxic (vitamin B4 RDA – 550mg)
- Produced on Mt scale (chicken feed additive) hence costs about 2 Euro/kg
- Non-toxic and biodegradable



Ionic Liquids

Choline like cations with various complexing agents



- Type I $Y = MCl_x, M = Zn, Sn, Fe$
- Type 2 $Y = MCl_x \cdot yH_2O$
- Type 3 $Y = RZ, Z = CONH_2, COOH, OH$

Studied far less than imidazolium based liquids
but already over 70 publications

Type I: Metal Salts



Metal containing ionic liquids

- Aluminium based ionic liquids well known
- Ionic liquids can also be formed with ZnCl_2 , SnCl_2 and FeCl_3
- Easy to make
- Do not react with water
- $\text{ChCl} + 2\text{ZnCl}_2 \rightarrow \text{Ch}^+ \text{Zn}_2\text{Cl}_5^-$

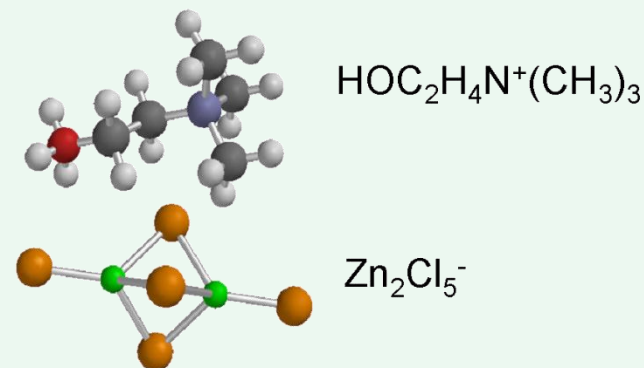


Table 1. Freezing Points for 1:2 QAS/Metal Halide Ionic Liquids

R_1	R_2	R_3	R_4	anion	metal halide	$T_f/^\circ\text{C}$
Me	Me	Me	$\text{C}_2\text{H}_4\text{OH}$	Cl^-	ZnBr_2	38
Me	Me	Me	$\text{C}_2\text{H}_4\text{OH}$	Cl^-	FeCl_3	65
Me	Me	Me	$\text{C}_2\text{H}_4\text{OH}$	Cl^-	SnCl_2	37
Me	Me	Me	$\text{C}_2\text{H}_4\text{OC}(\text{O})\text{Me}$	Cl^-	ZnBr_2	48
Me	Me	Me	$\text{C}_2\text{H}_4\text{OC}(\text{O})\text{Me}$	Cl^-	SnCl_2	20
Me	Me	Me	$\text{C}_2\text{H}_4\text{Cl}$	Cl^-	SnCl_2	63
Me	Me	benz	$\text{C}_2\text{H}_4\text{OH}$	Cl^-	SnCl_2	17
Me	Me	benz	$\text{C}_2\text{H}_4\text{OH}$	Cl^-	FeCl_3	21

Physical Properties

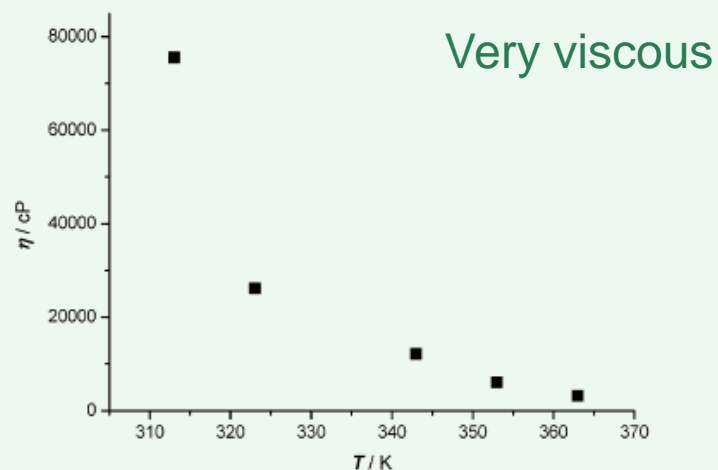


Figure 4. Viscosity of a 2 ZnCl₂/1 ChCl mixture as a function of temperature.

Mono and di-metallic species dominate

ZnCl₂ and SnCl₂ do not form Lewis basic liquids

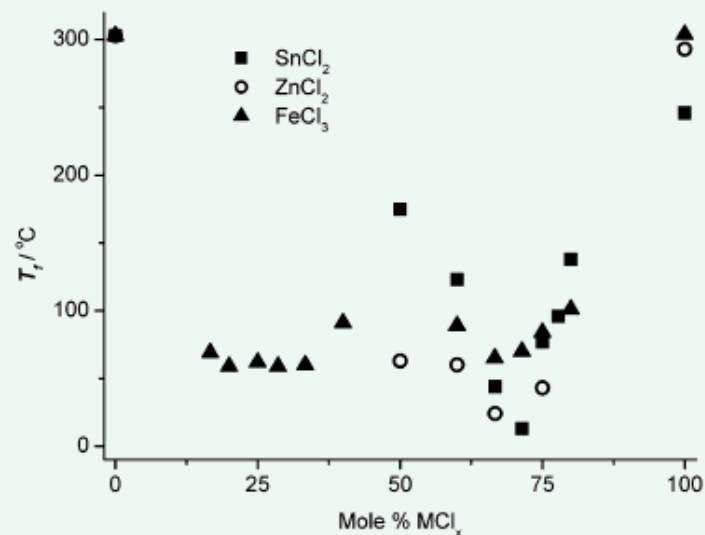


Figure 1. Freezing point for the ZnCl₂/ChCl and SnCl₂/ChCl systems as a function of composition.

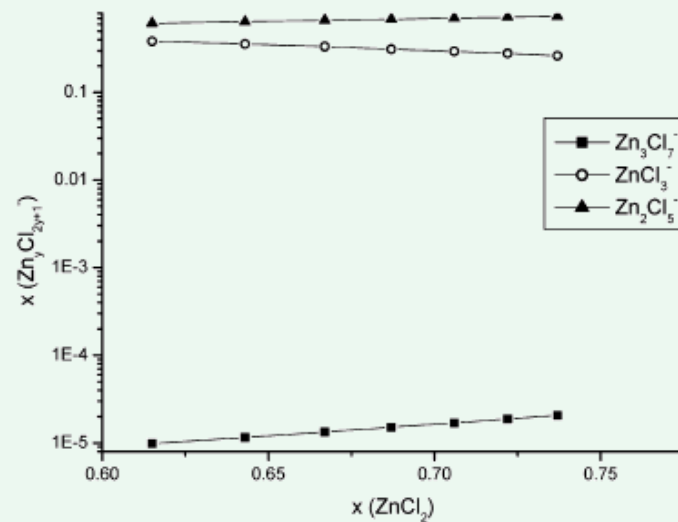


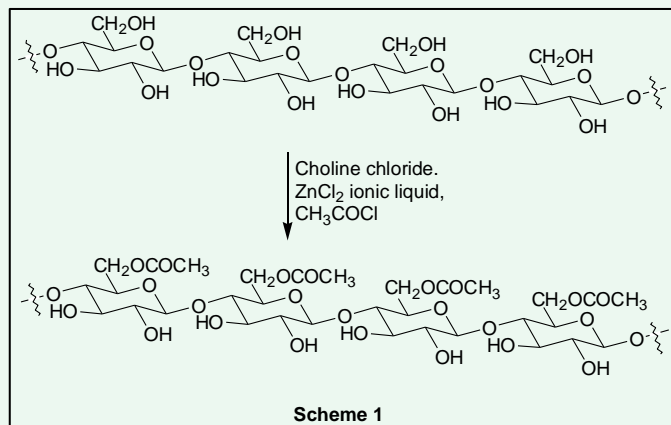
Figure 3. Mole fraction of chlorozincate anions in a choline chloride/zinc chloride ionic liquid as a function of composition at 60 °C.

Lewis Acid Catalysed Reactions

- Friedel Crafts
- Diels Alder
- Fisher Indole
- Acetylation of cellulose

Advantages:

- Products form separate phase - can be decanted/distilled from the ionic liquid
- No solvent residues
- High yields
- High regioselectivity



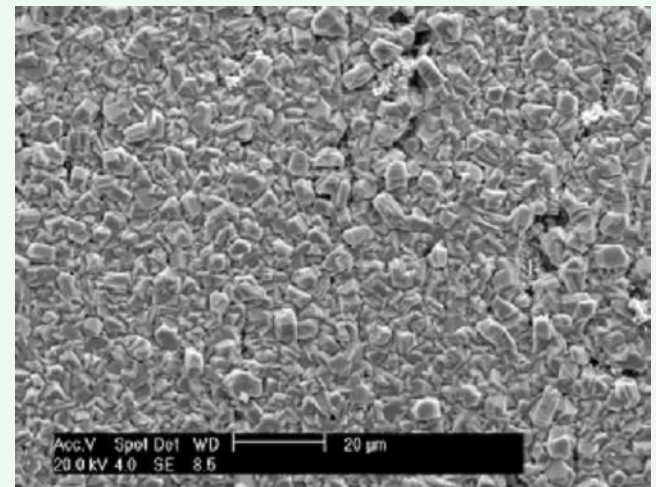
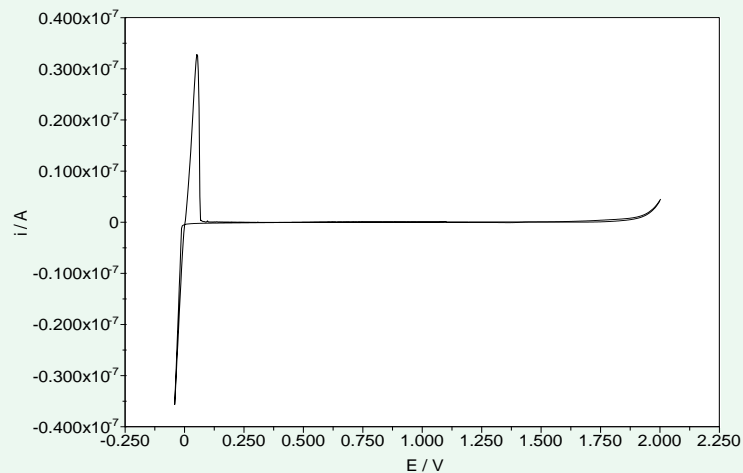
Abbott et al. Green Chem., 2002, 4, 24.

Abbott et al. Green Chem., 2005, 7, 705.

Morales et al. Chem. Commun., 2004 158

Zinc Deposition - IL

- High current efficiency (>99%) (no $\text{H}_2\uparrow$)
- Zinc deposition almost totally reversible (soluble anodes)
- Deposition of alloys possible
- Non-microcracked deposit
- High corrosion resistance

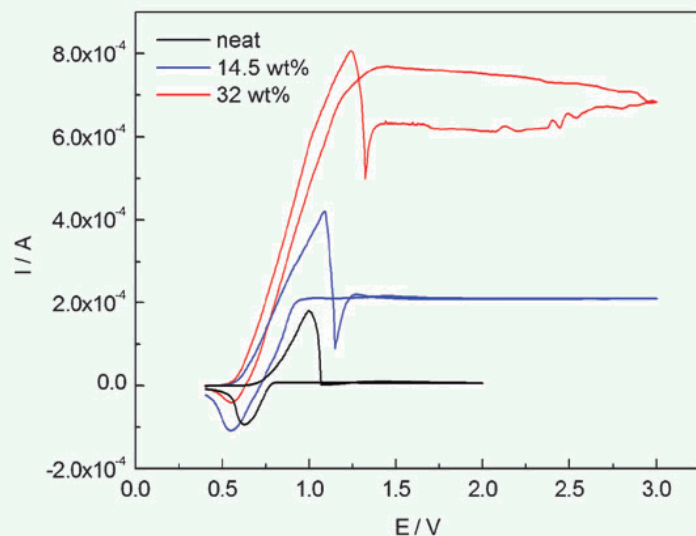
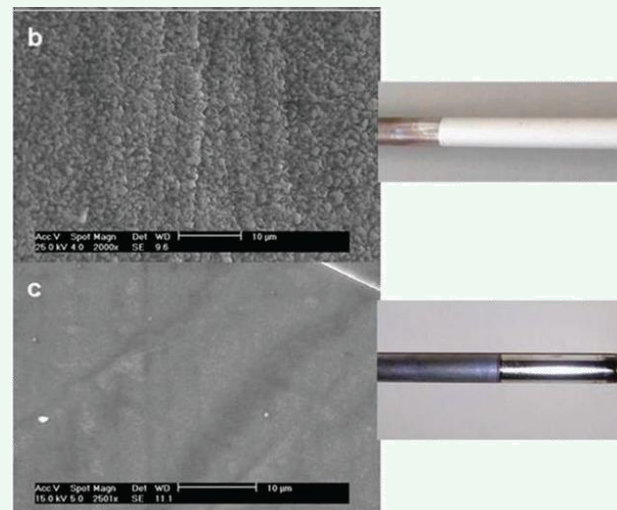


Abbott et al. Trans IMF, 2001 79,204.

Chloroaluminate systems still being

System affected by;

- Mass transport
- Added electrolyte
- Speciation
- Anode material



Aluminium Deposition

- Mirror finish can be obtained
- 35 L Pilot plant now being operated
- New IP uses no QAS



Type 2: Hydrated Metal Salts
 $R_1R_2R_3R_4N^+ X \cdot zY \quad Y = MCl_x \cdot yH_2O$

Hydrated Salt Mixtures

- Developed to incorporate other metals into ionic liquids
- Mixture of quaternary ammonium salts with a hydrated metal salt
- Does not form liquid with all salts
- No 'free' water molecules
- A lot less viscous than Type I

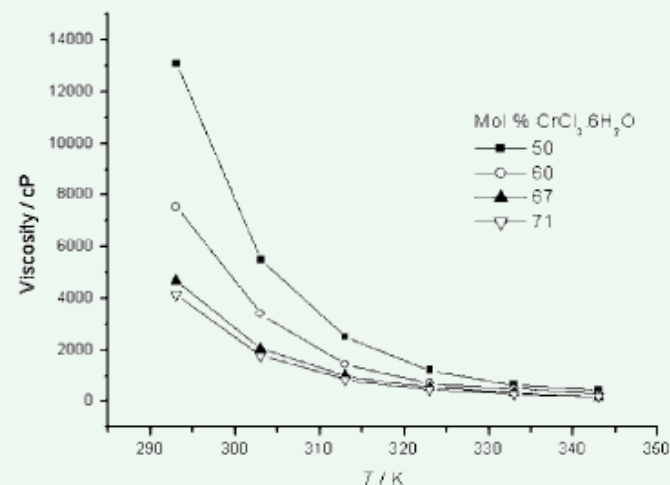


Figure 1. Viscosity of ChCl/CrCl₃·6H₂O mixtures as a function of temperature and composition

Hydrated Salt Mixtures

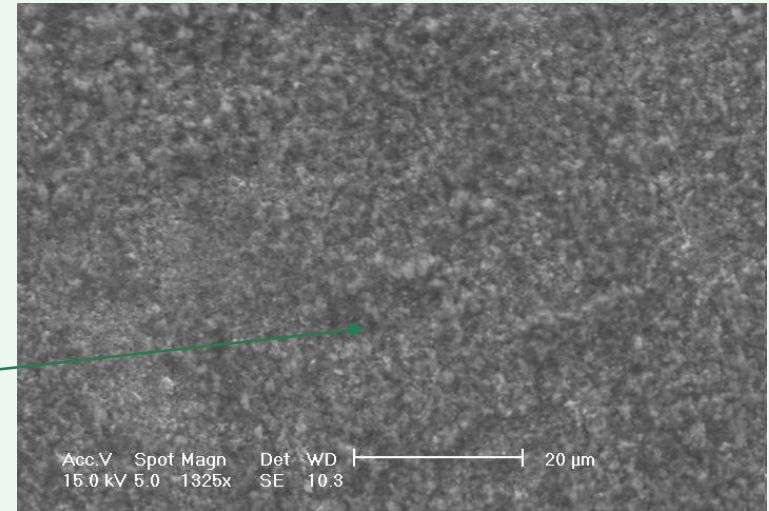
- Applicable to a wide range of other metals in various oxidation states

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Hydrated Salt	f.p / °C
$\text{CrCl}_3 \cdot 6\text{H}_2\text{O}$	4
$\text{CaCl}_2 \cdot 6\text{H}_2\text{O}$	5
$\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$	10
$\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$	16
$\text{LaCl}_3 \cdot 6\text{H}_2\text{O}$	6
$\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$	48

Chromium Plating

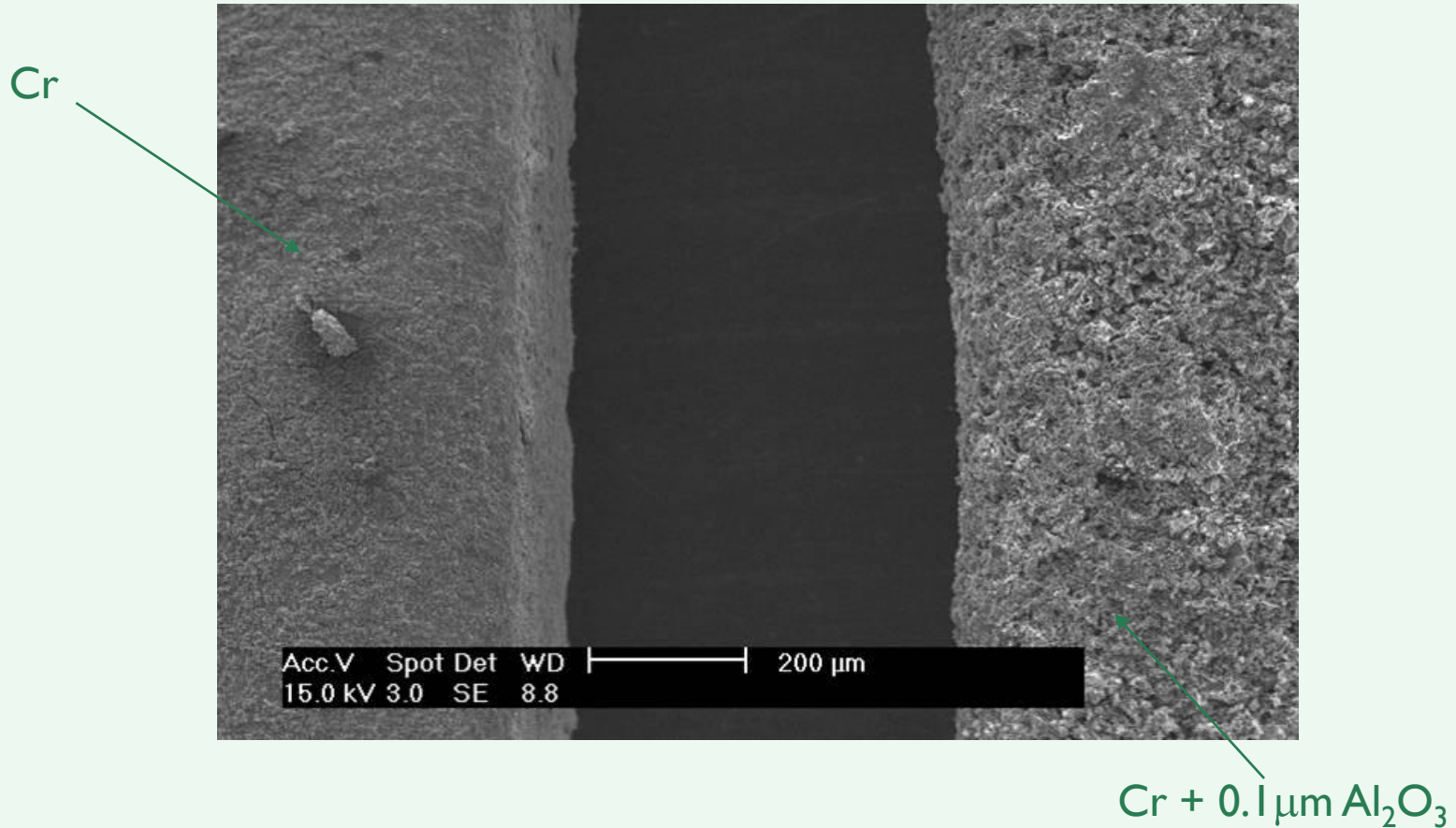
- ❑ Negligible hydrogen evolution
- ❑ High current efficiency (>90%)
- ❑ Uses Cr(III) (less toxic, less e^-)
- ❑ Non microcracked deposit
- ❑ Soluble anodes



SEM image of the deposit formed following the electrolysis of the ChCl : $2\text{CrCl}_3 \cdot 6\text{H}_2\text{O}$ system containing 10 wt% LiCl at 60 °C for 2 hours onto a nickel electrode at a current density of 0.345 mAcm^{-2} .

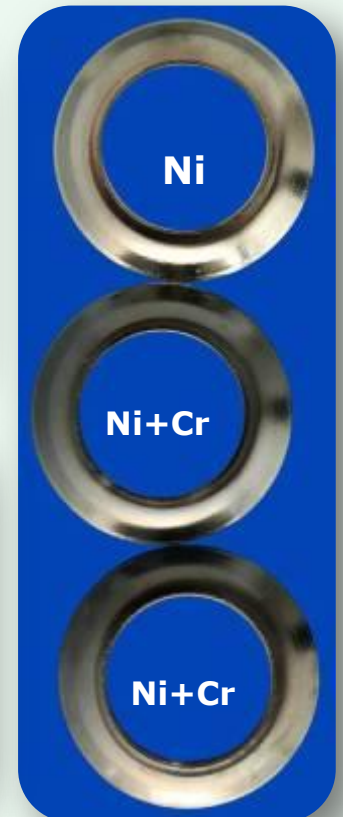
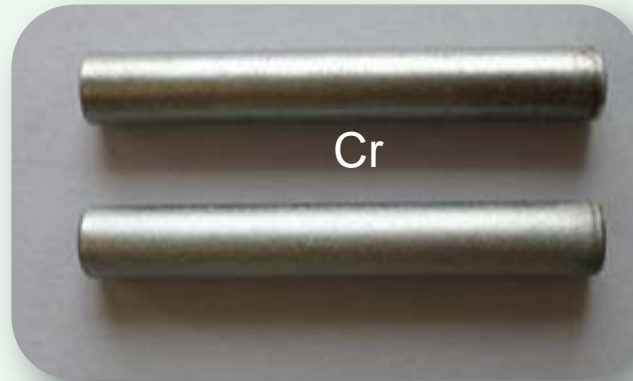
Composite Materials

- ❑ Stable colloidal suspensions can be made and these can be incorporated into metallic coatings



Chromium Plating

- New formulations have led to bright Cr deposits.
- Surfaces can be ground - good adhesion



Chromium Plating

- Improved current efficiency (economic benefit)
- Less toxic components – non-corrosive (social benefit)
- Improved product (market benefit)
- Recyclable bath (environmental benefit)
- More versatile substrates (larger market)

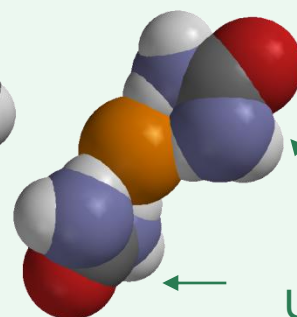
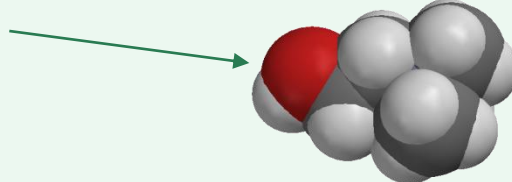
Type 3: Hydrogen Bond Donors



Deep Eutectic Solvents

□ Many HBDs are INEXPENSIVE (c.a. £1/kg), Non-toxic, Non-flammable, Biodegradable, Versatile ($>10^5$ liquids), Unusual solvent properties.

Choline chloride – A vitamin in chicken feed



Urea – A common fertiliser



Acids



Amides



Alcohols

□ Dissolve a wide range of solutes
e.g. salts, polar organics, metal
oxides, amino acids, enzymes and
surfactants.

Deep Eutectic Solvents

Hydrogen bond donor	Fr Pt. /°C
Amides	
Urea, NH_2CONH_2	12
Acetamide, CH_3CONH_2	51
Thiourea, NH_2CSNH_2	69
Acids	
Trichloroacetic acid $\text{Cl}_3\text{CCO}_2\text{H}$	-24
Phenylacetic acid $\text{C}_6\text{H}_5\text{CH}_2\text{CO}_2\text{H}$	-5
Malonic acid, $\text{HO}_2\text{CCH}_2\text{CO}_2\text{H}$	3
Oxalic Acid, $\text{HO}_2\text{CCO}_2\text{H}$	13
<i>p</i> -Toluene sulfonic acid $\text{CH}_3\text{C}_6\text{H}_4\text{SO}_3\text{H}$	27
Alcohols	
<i>m</i> – Cresol, $\text{CH}_3\text{C}_6\text{H}_4\text{OH}$	< -35
Phenol $\text{C}_6\text{H}_5\text{OH}$	-30
Ethylene glycol	-10
Glycerol	-20
D (-) Fructose, $\text{C}_6\text{H}_{12}\text{O}_6$	5

Solvent properties can be markedly changed by altering the HBD

Freezing points of mixtures of hydrogen bond donors with choline chloride in a 2:1 ratio.

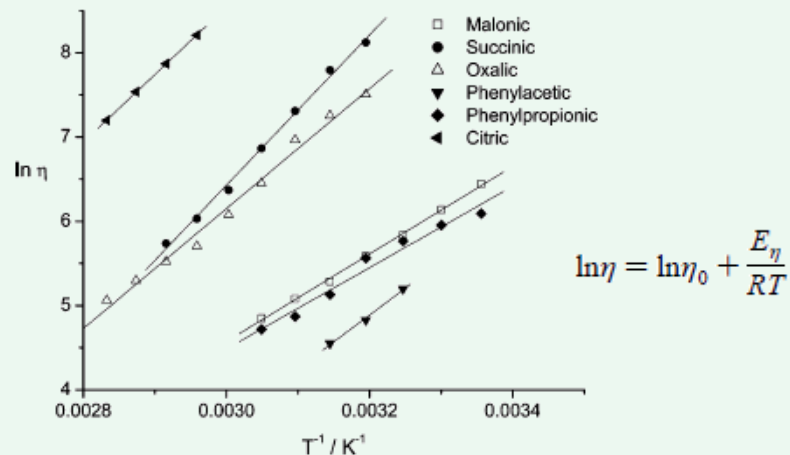


Figure 4. Plot of log viscosity vs. reciprocal of temperature for a variety of DES.

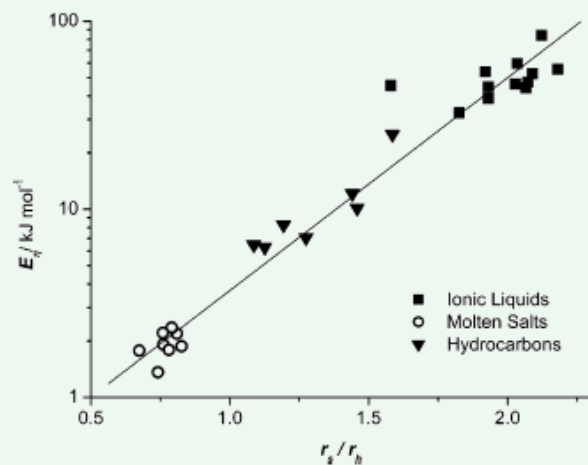


Figure 6. Energy for activation of viscous flow as a function solvent to hole radius ratio.

Activation energy for viscous flow related to size of the ion and void volume

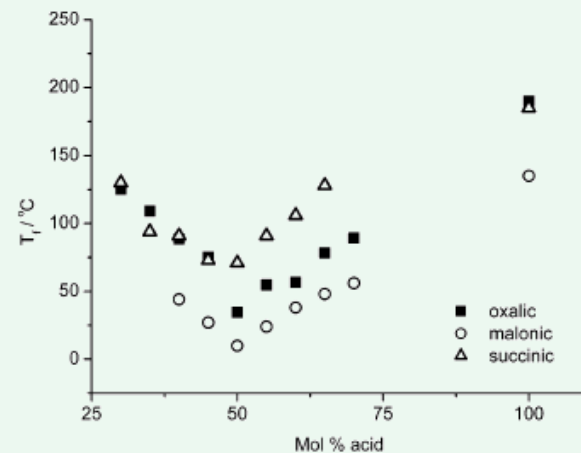


Figure 2. Freezing points of choline chloride with oxalic, malonic, and succinic acids as a function of composition.

Eutectic point occurs at 1:1 composition for bifunctional molecules

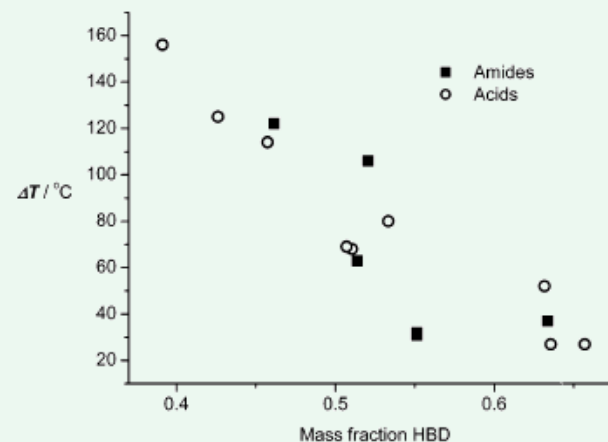


Figure 3. Freezing point depression for the eutectic mixtures listed in Table 1 and reported in the literature¹⁰ as a function of mass fraction of HBD.

Depression of freezing point related to the amount of HBD

Product	Complexing agent
Reline	Urea
Maline	Malonic acid
Oxaline	Oxalic acid
Glyceline	Glycerol
Ethaline	Ethylene Glycol
Chromeline	$\text{CrCl}_3 \cdot 6\text{H}_2\text{O}$

Many products require a mixture of complexing agents to get the right properties.

Can be made easily on a large scale.



1.3 tonnes of Ethaline

Metal Deposition

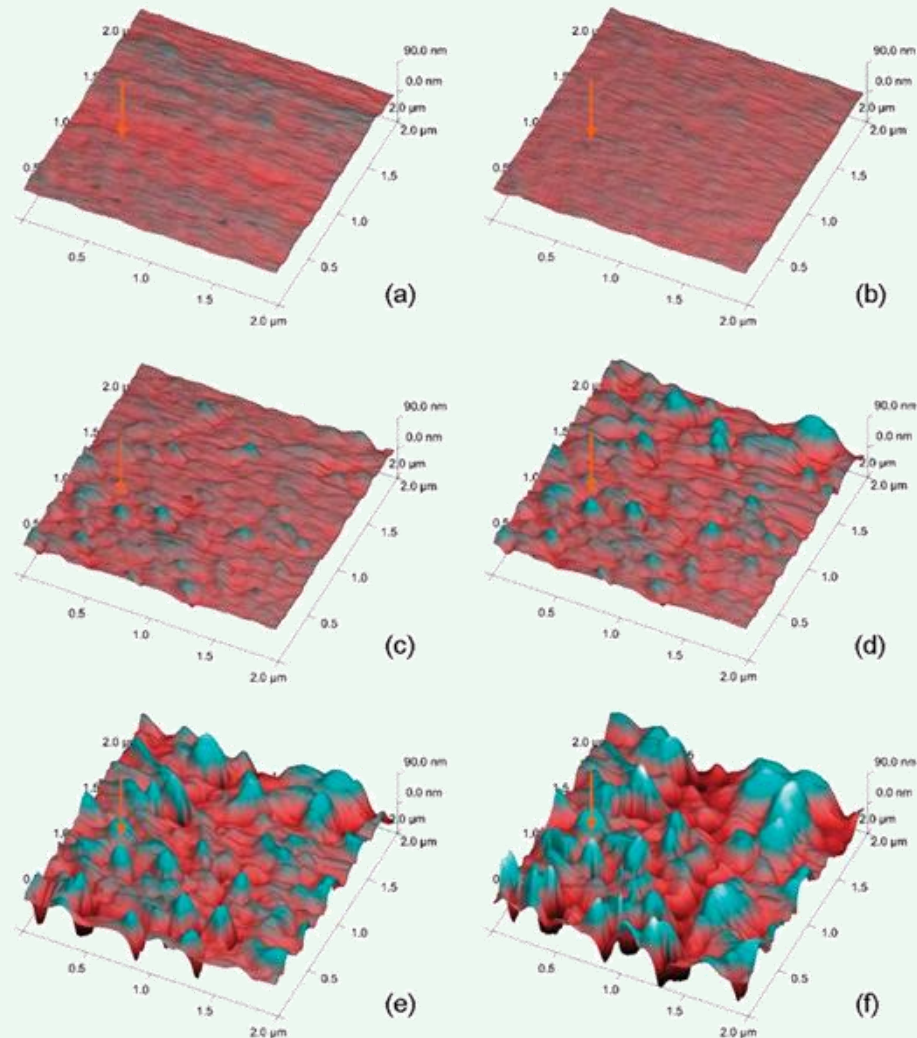
- A range of metals and alloys have been deposited from these ionic liquids

I																	18	
H	2												13	14	15	16	17	He
Li	Be											B	C	N	O	F	Ne	
Na	Mg	3	4	5	6	7	8	9	10	11	12	Al	Si	P	S	Cl	Ar	
K	Ca	Sc	Ti	V	Cr	Mn	Fe	Co	Ni	Cu	Zn	Ga	Ge	As	Se	Br	Kr	
Rb	Sr	Y	Zr	Nb	Mo	Tc	Ru	Rh	Pd	Ag	Cd	In	Sn	Sb	Te	I	Xe	
Cs	Ba	La	Hf	Ta	W	Re	Os	Ir	Pt	Au	Hg	Tl	Pb	Bi	Po	At	Rn	
Fr	Ra	Ac																

Ce	Pr	Nd	Pm	Sm	Eu	Gd	Tb	Dy	Ho	Er	Tm	Yb	Lu
Th	Pa	U	Np	Pu	Am	Cm	Bk	Cf	Es	Fm	Md	No	Lr

Nucleation mechanism

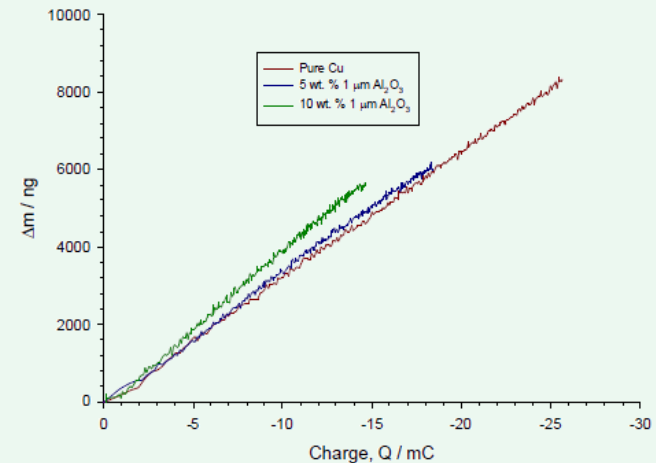
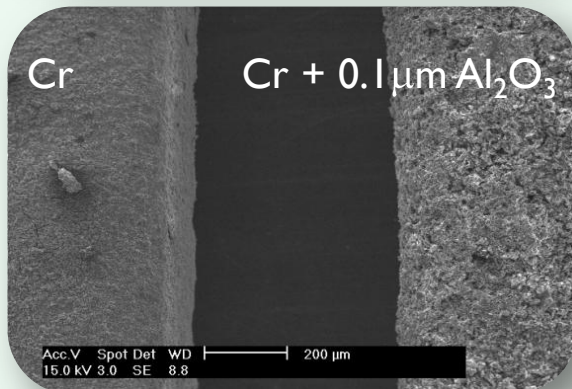
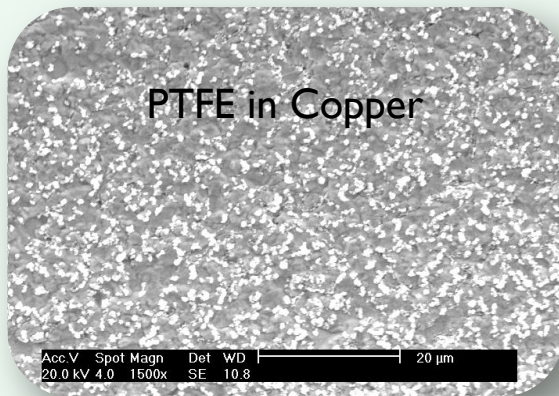
- Mechanistic study using in situ AFM/QCM
- Now using DHM to improve time resolution
- Studied Ag, Cu, Zn and Ni



Smith et al. Anal. Chem. (2009), 81, 8466

Composite Materials

- Stable colloidal suspensions can be made and these can be incorporated into metallic coatings

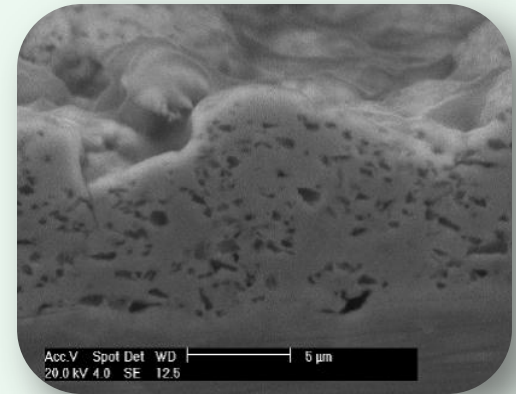
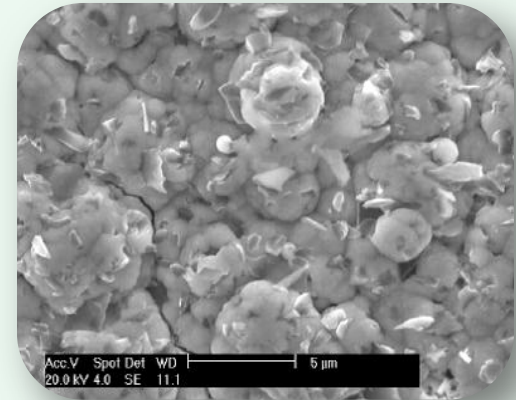
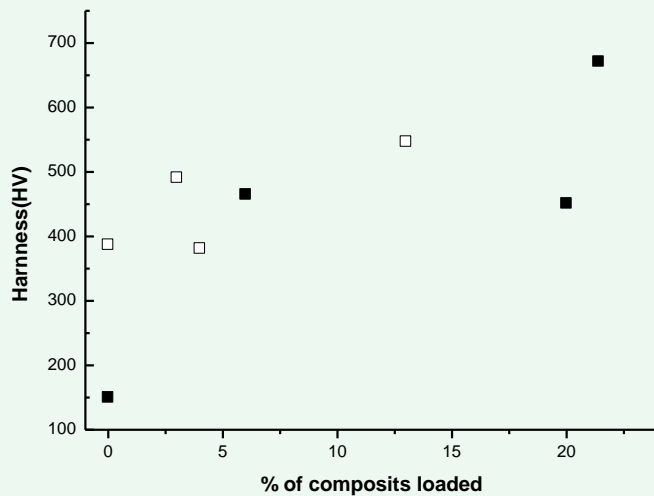


Wt % Al ₂ O ₃ in solution	Wt % Al ₂ O ₃ in coating	
	0.05 μm particles	1 μm particles
0.5	0.7	2.0
5	3.3	3.5
10	27.3	23.0

Abbott et al. *Phys. Chem. Chem. Phys.*, 2009, 11, 4269
 Martis, et al *Electrochim. Acta* 2010, 55, 5407

Nickel composite deposition

- Deposition of composites
- Even distribution of particulates
- Increase in material hardness and wear resistance



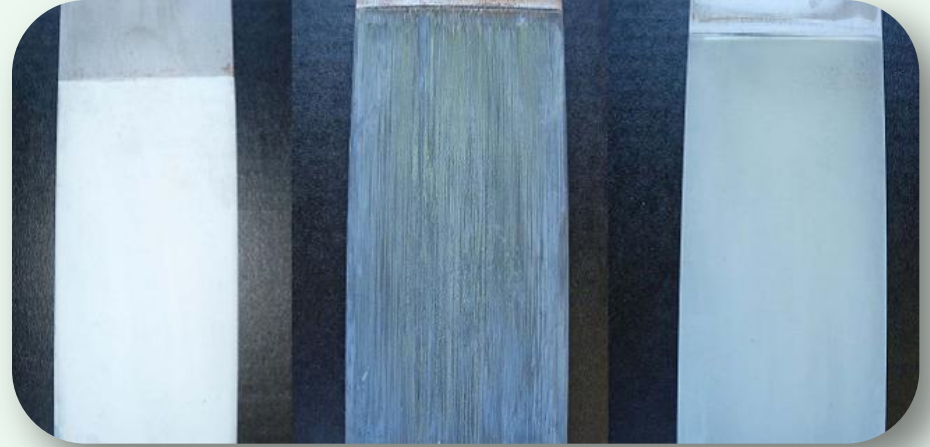
Alloy deposition

- Zn and a range of Zn alloys (Cu, Fe, Ni and Sn) were successfully deposited and the systems characterised
- Scale up the processes to a large laboratory scale, real parts coated and post treatment finishes applied
- Major focus on **ZnSn** alloys due to their potential for Cd replacement

Zn Alloys



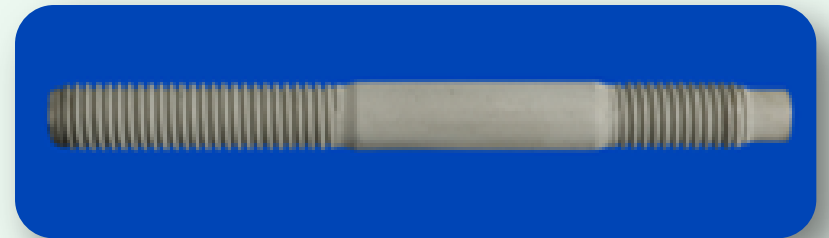
ZnSn on 10 mm rods



Zn, ZnNi and ZnSn on plates 150x80 mm

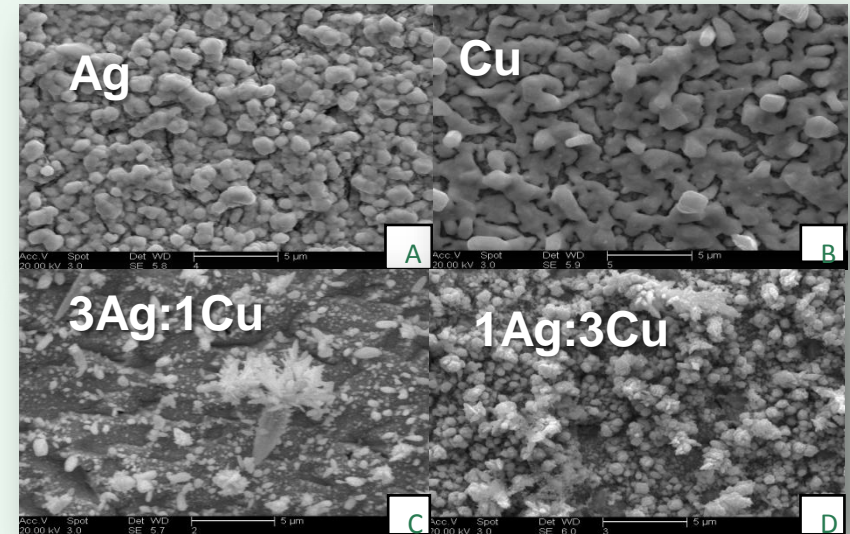
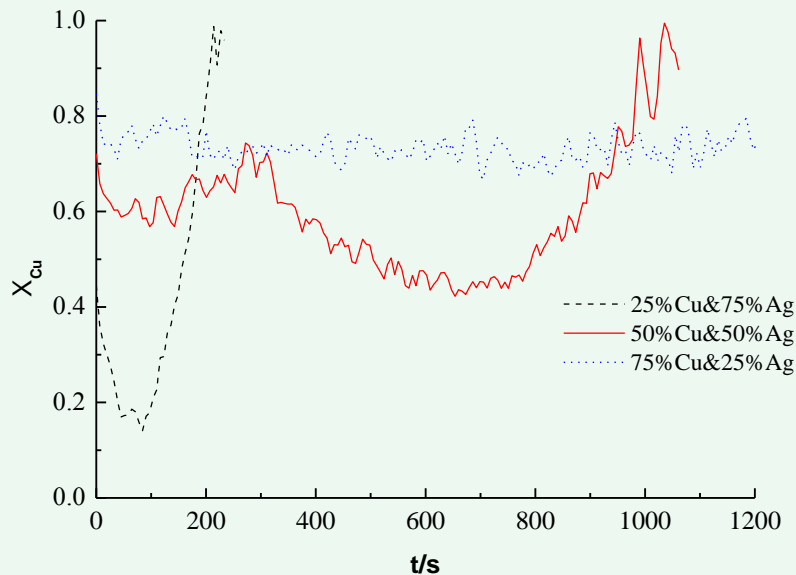


ZnSn on real parts



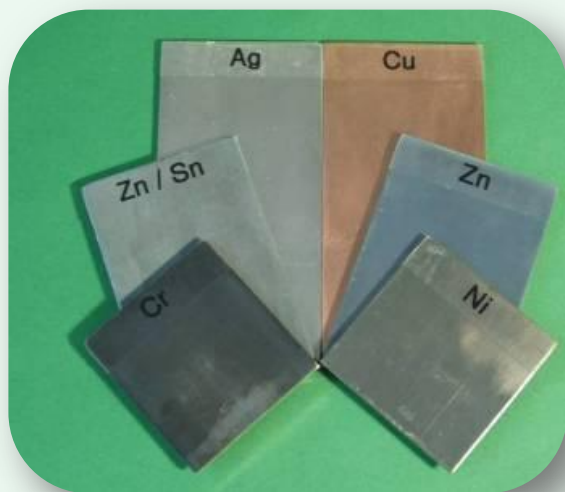
Copper Alloys

- Real time monitoring achieved using EQCM
- Currently studying mechanism of nucleation

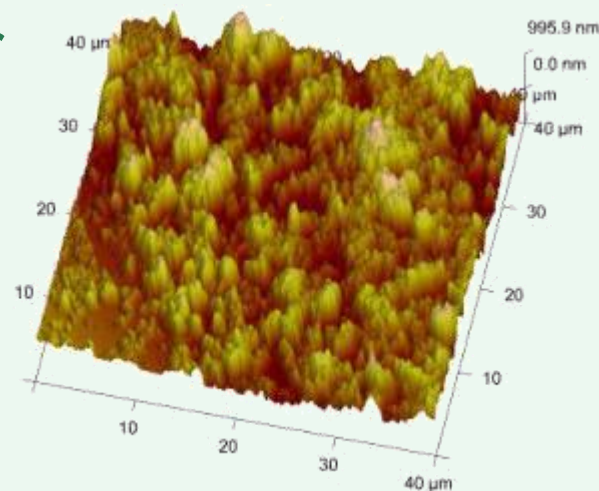
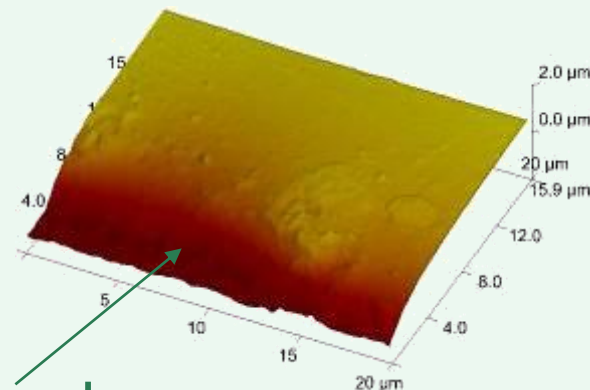


Brighteners

- Brighteners have been developed for a variety of metals



Cu deposited with and without brightener

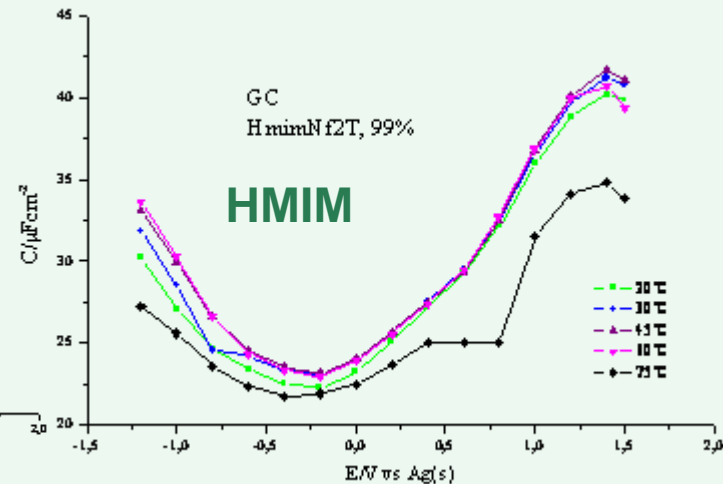
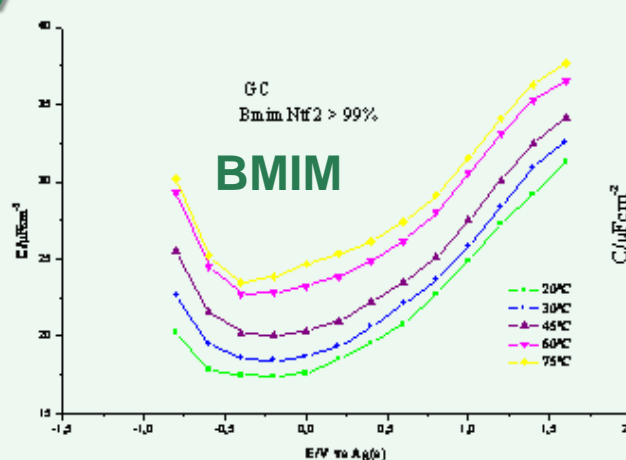


Mechanism is different for each metal and additive

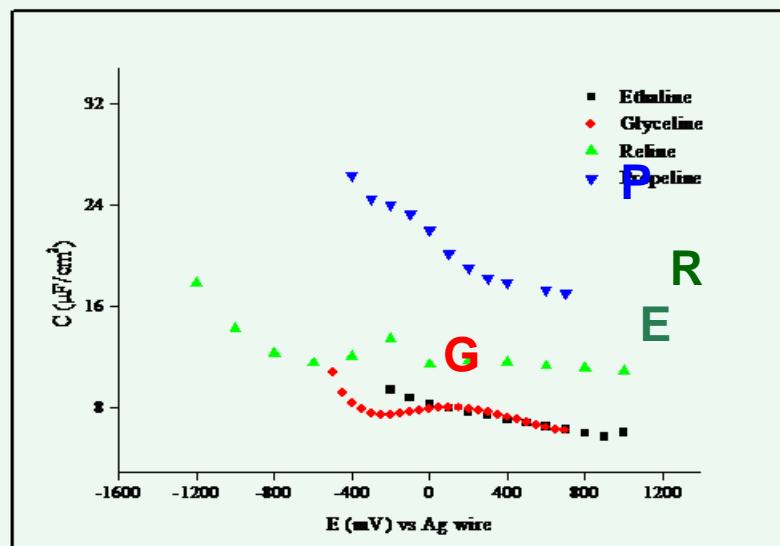
- Some work by changing double layer properties
- Others change speciation and redox potentials

Double layer

Imidazolium based ionic liquids



Nucleation depends upon complex charge and reduction potential



Capacitance – potential curves for different liquids

Speciation

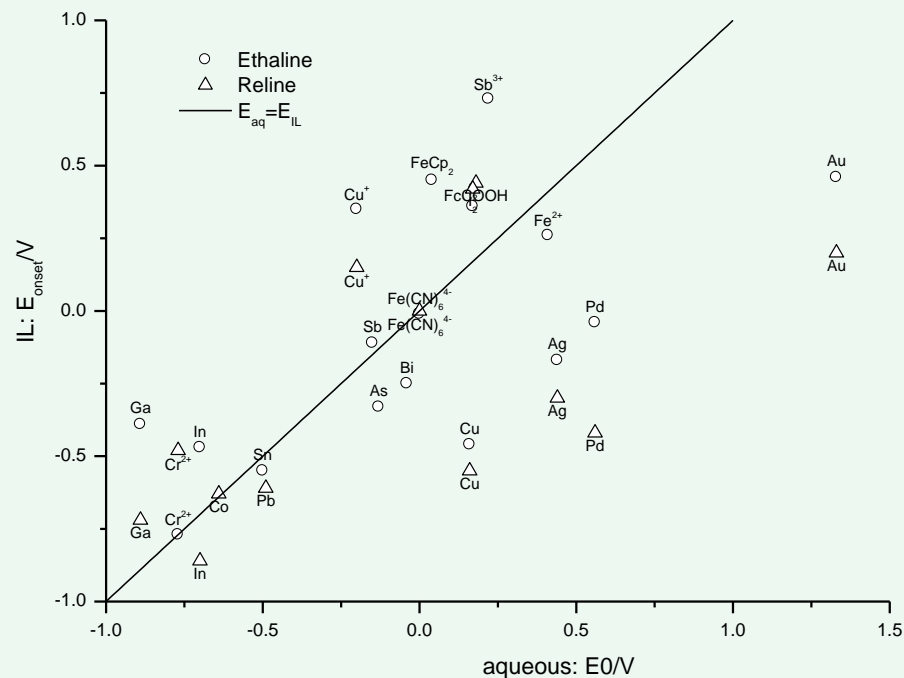
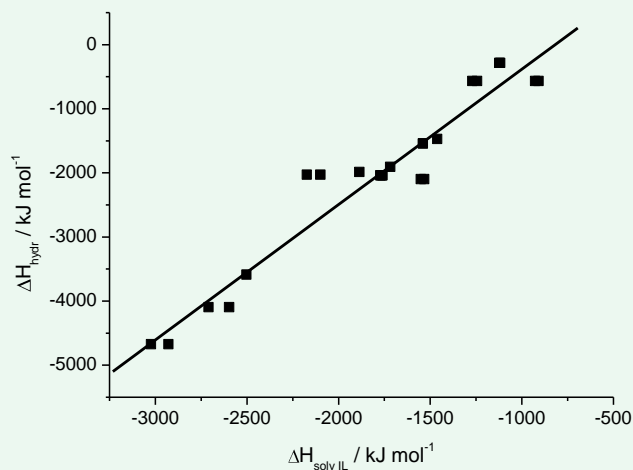
- Speciation affects redox potentials
- Recently studies EXAFS of Zn, Ni and Cu in Reline and Ethaline
- Unusual results



Cu^{2+} in various ionic liquids and Deep Eutectic Solvents.

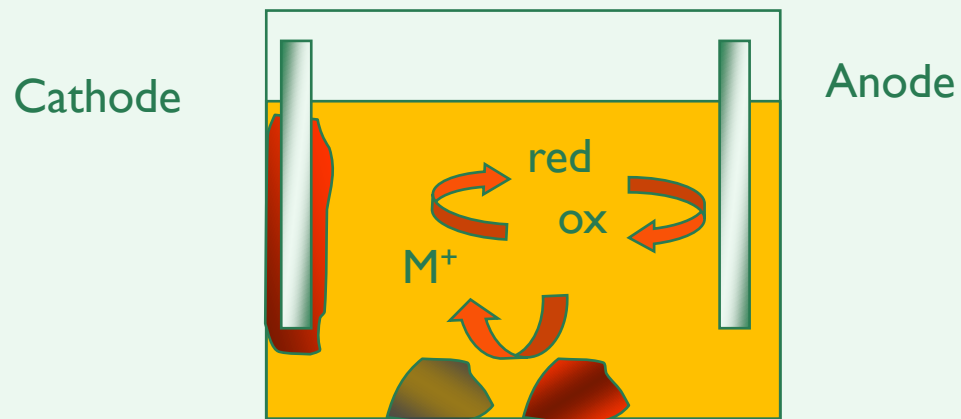
Comparison of $E_{1/2}$ values

- Electrochemical series constructed
- Enthalpies of solvation calculated
- Good correlation with enthalpy of hydration



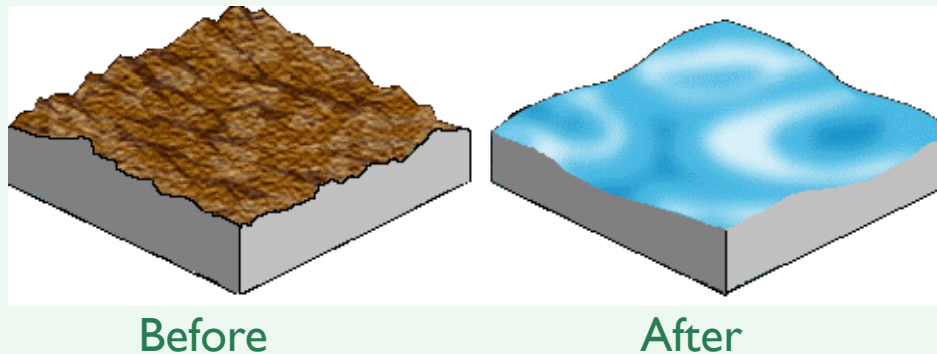
Electrocatalysis

- New methodology developed for oxidation of metals from native state.
- Has been applied to mixtures of metals
- Electrocatalytic oxidation of metals has been achieved
- Quantitative separation of Cu from Zn has been demonstrated.



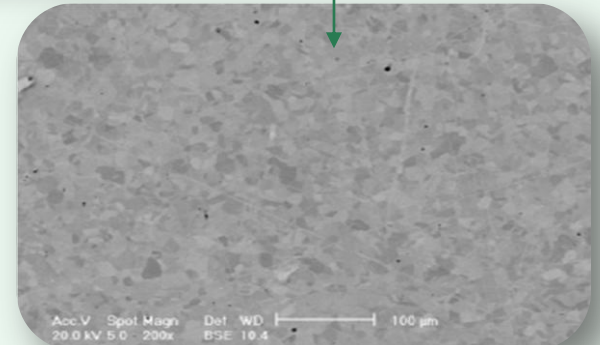
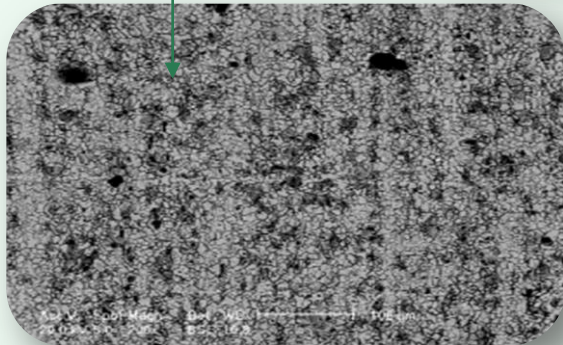
Electropolishing

- Large worldwide industry - mostly stainless steel
- Opposite to electroplating i.e. dissolves metal off
- Decreases wear and improves corrosion resistance
- Uses sulphuric and phosphoric acids ($\text{HF} + \text{CrO}_3$)
- Low current efficiency (10 – 20%)



Pre-polished

Electropolished



Scale-up

Standard tank, pump and fittings (PE, PP and nylon)



Stainless steel cathodes

Titanium anode jig

Negligible gassing at anode

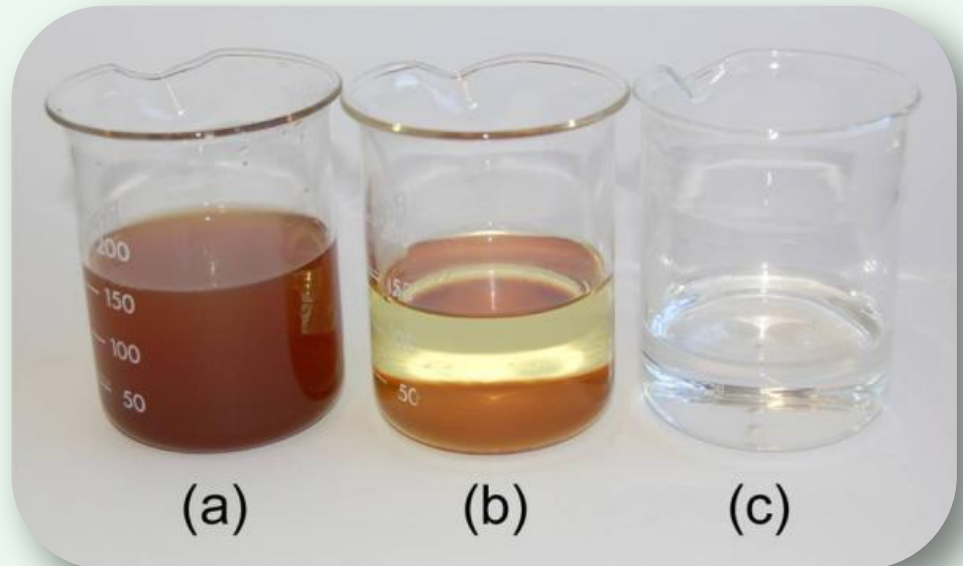


Currently operating on 1300 kg at Anopol in Birmingham

Recycling

- Liquid fully recyclable
- Spent Ethaline from the electropolishing process
- Equal volumes of water added (b) and then distilled off (c)

Metal	Saturation conc. / ppm
Iron	66746
Chromium	9150
Nickel	3135

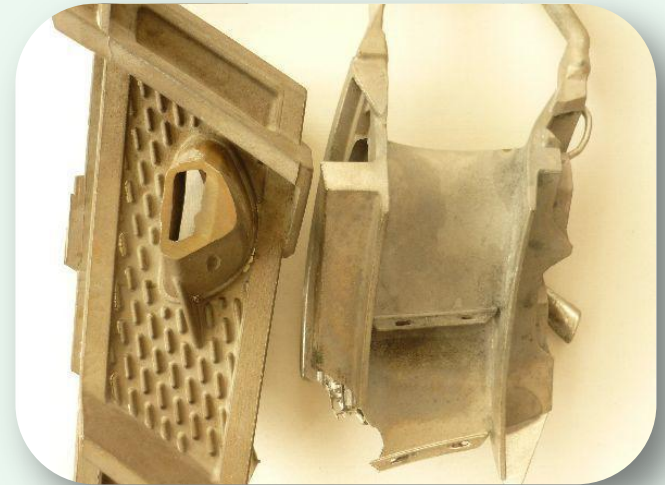
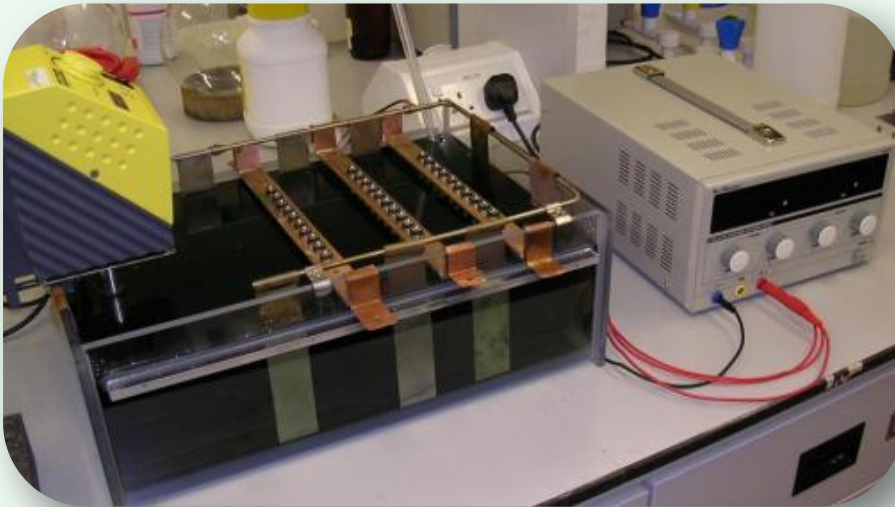


Electropolishing

- Better surface finish (market)
- Non-corrosive (social)
- Benign liquid – ChCl /glycol (social)
- Improved current efficiency ($>80\%$) (economic)
- Less gas evolution (environmental)
- Metal recoverable (environmental)
- Costs comparable with aqueous processes ($0.17 \text{ Euro/ m}^{-2}$)

Electropolishing

- New market developed for super-alloy polishing



Automatic polishing line at Anopol.

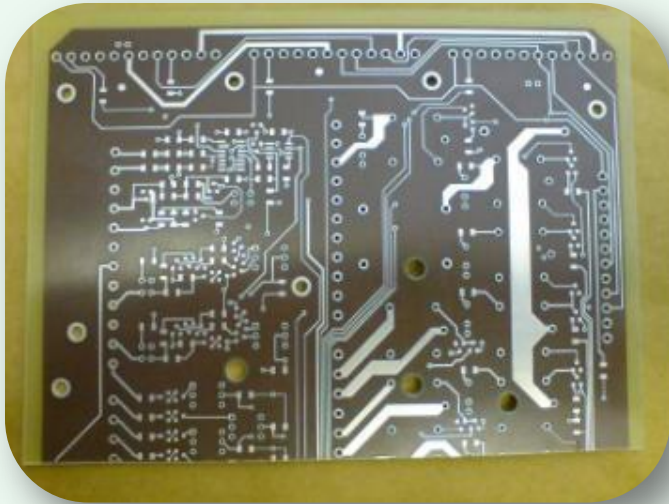


Polishing line at UoL.



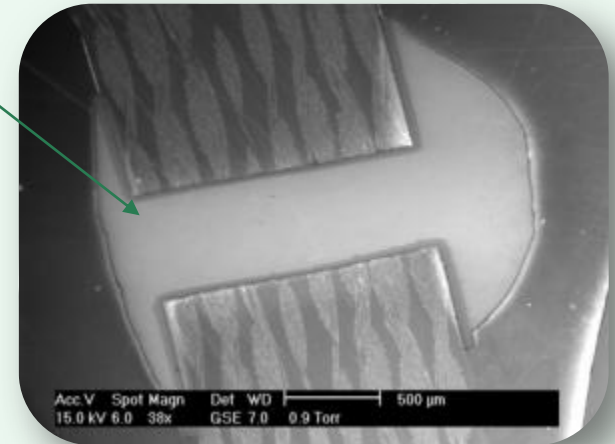
Batch polished steering wheel encoder disks

□ Can also be used for electroless plating – Silver deposition



P.W. CIRCUITS LTD

Soldering Ag coated Cu interconnects



Currently being commercialised in Leicester

- ❑ Silver deposition process currently being scaled up
- ❑ PCB line now installed in Leicester



Abbott et al. PhysChemChemPhys 2007, 9, 3735
Smith et al. CircuitWorld 2010, 36, 3



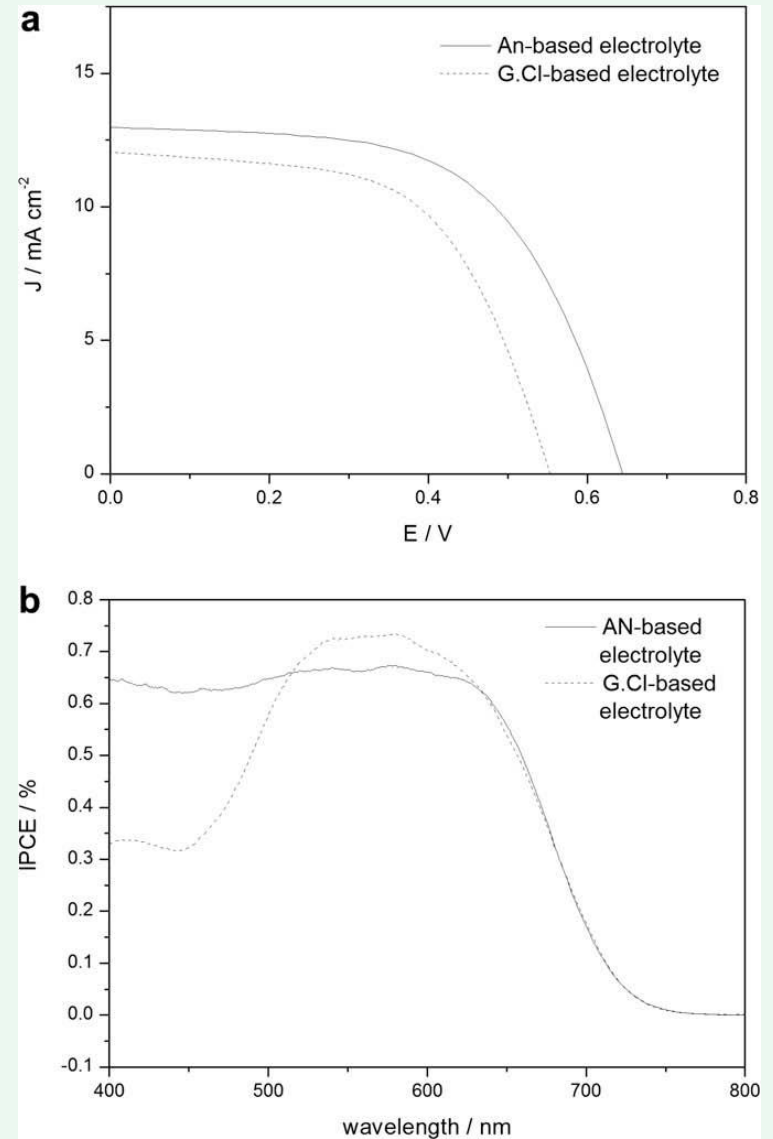
ild
ionic liquid demonstrator



Dye Sensitise solar Cell

Uses Chl and glycerol in a Graetzel cell

Results compare well with acetonitrile based electrolyte

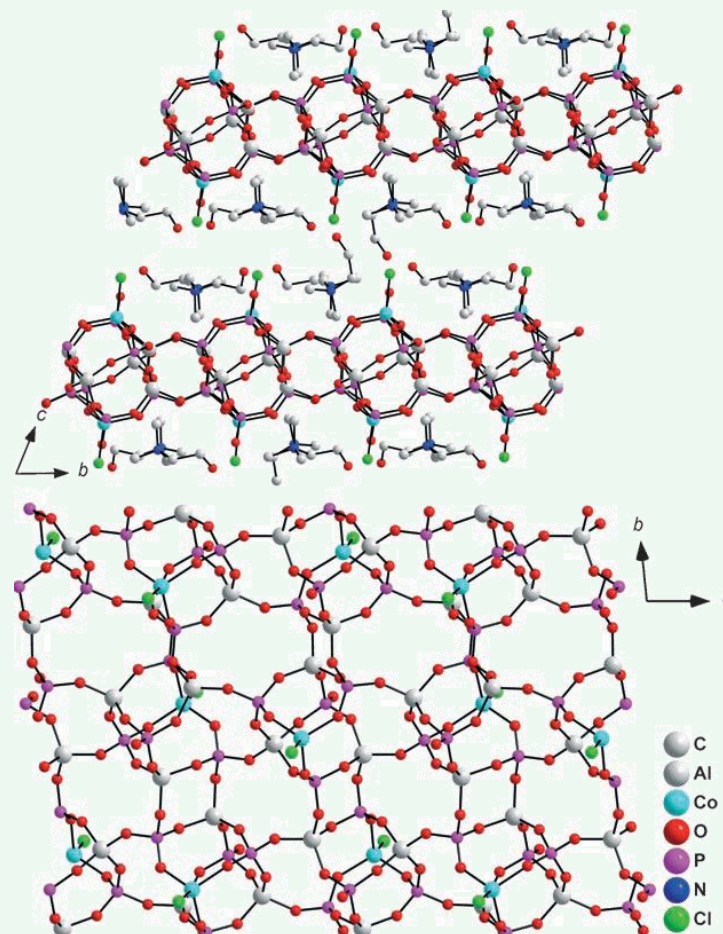


Ionothermal synthesis of zeolites

Cation of the DES acts as the structure-directing template

Synthesis of SIZ-14:

The ChCl: succinic acid (4 g),
 aluminum isopropoxide (0.22 g), phosphoric acid
 (0.32 g, 85 wt% in water,) cobalt acetate
 tetrahydrate (0.21 g)
 cyclam (0.15 g)
 teflon-lined autoclave.
 Mixture was heated at 180°C for 3 days.



Urea Choline Chloride

Wide range of solutes show high solubilities

In general those capable of forming H bonds show the highest solubilities.

Solute	Solubility / mol/l
Lithium chloride	>2.5
Silver Chloride	>0.66
D-alanine	>0.38
benzoic acid	>0.82
Copper (I) oxide	>0.11
Calcium carbonate	>0.21
SDS	>0.36

Urea Choline Chloride

Wide range of solutes show high solubilities e.g. metal oxides



Dissolved oxides can be recovered electrochemically

High solubility demonstrated for a range of metal oxides

Metal Oxide	M.pt. / °C	Solubility / ppm
Al ₂ O ₃	2045	<1
CaO	2580	6
CuO	1326	470
Cu ₂ O	1235	8725
Fe ₂ O ₃	1565	49
Fe ₃ O ₄	1538	40
MnO ₂	535	493
NiO	1990	325
PbO ₂	888	9157
ZnO	1975	8466

Solubility of metal oxides in a 2:1 urea: choline chloride eutectic at 60 °C.

Tunable Metal Oxide Solubility

	Solubility / mol dm ⁻³		
	CuO	Fe ₃ O ₄	ZnO
I Malonic acid: I ChCl	0.246	0.071	0.554
I Oxalic acid: I ChCl	0.071	0.341	0.491
2Phenylpropionic acid: I ChCl	0.473	0.014	>0.491

EHF Dust

- ☐ EAF produces c.a. 15 - 20 kg of dust per tonne of steel.
- ☐ The dust is classed as a toxic waste because of the high heavy metal content.
- ☐ Several million tonnes of dust are produced per annum.
- ☐ Dust forms when volatile metals, e.g. Pb and Zn vaporise at the high operating T and are oxidized in the airflow through the furnace.



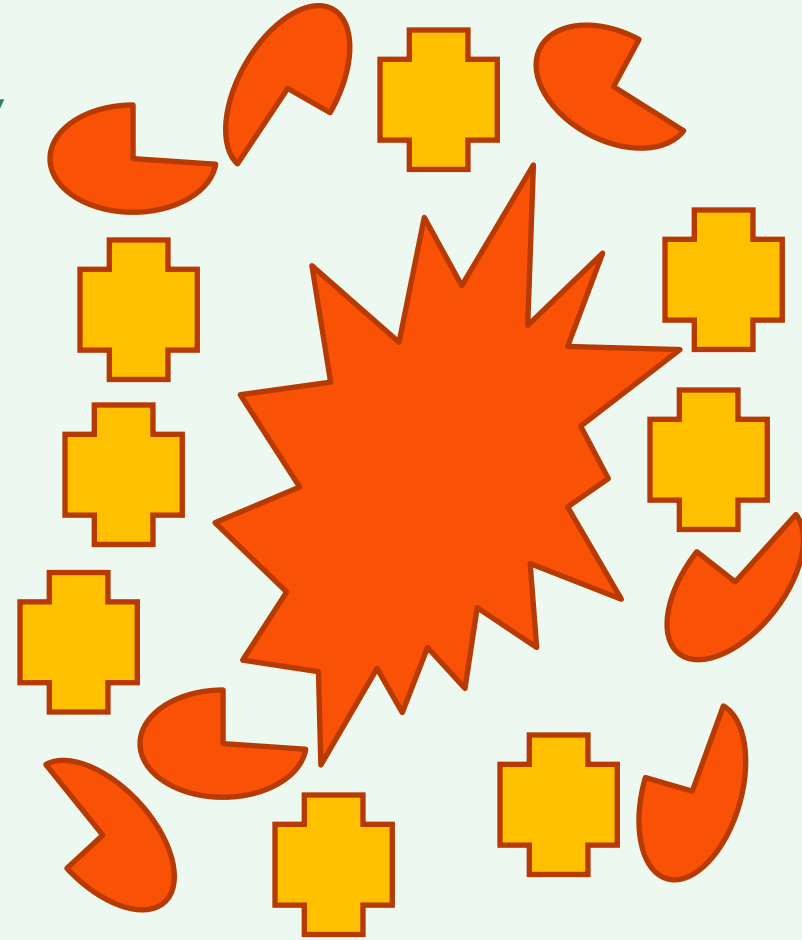
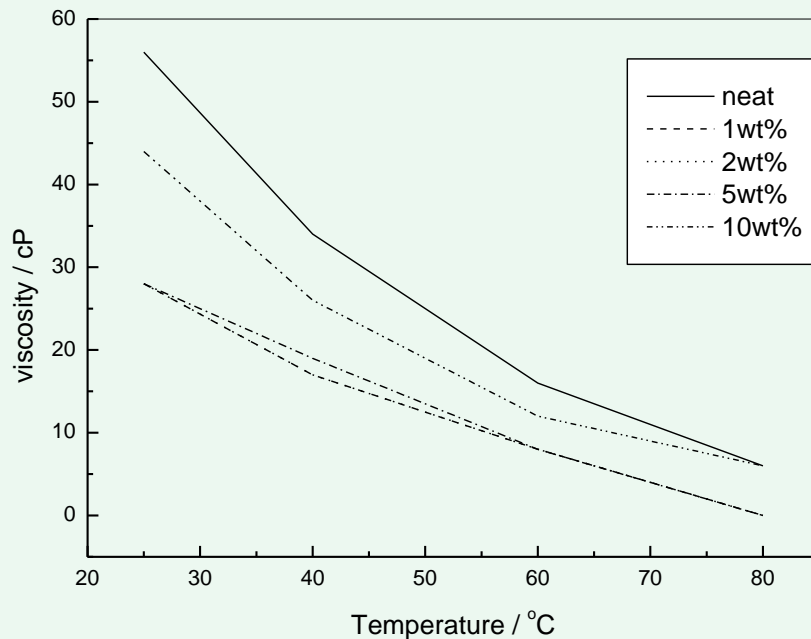
EAF Dust

Composition of EAF dust sample

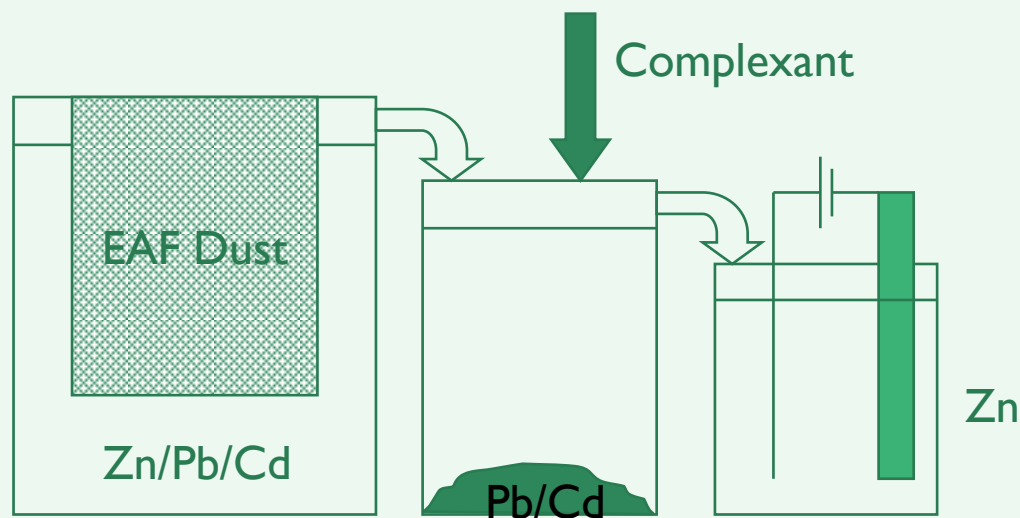
Metal	Content in EAF dust /wt %	Solubility of metal oxide /ppm	Solubility from EAF dust /ppm
Al	12	Al_2O_3 – < 1	<1
Cu	1	CuO - 470 Cu ₂ O - 8725	5
Fe	38	Fe ₂ O ₃ - 89 Fe ₃ O ₄ – 40	16
Mn	4.5	MnO ₂ – 493	-
Pb	4	PbO ₂ – 9157	113
Si	4	SiO ₂ - < 1	<1
Zn	33	ZnO – 8466	4288

Colloids

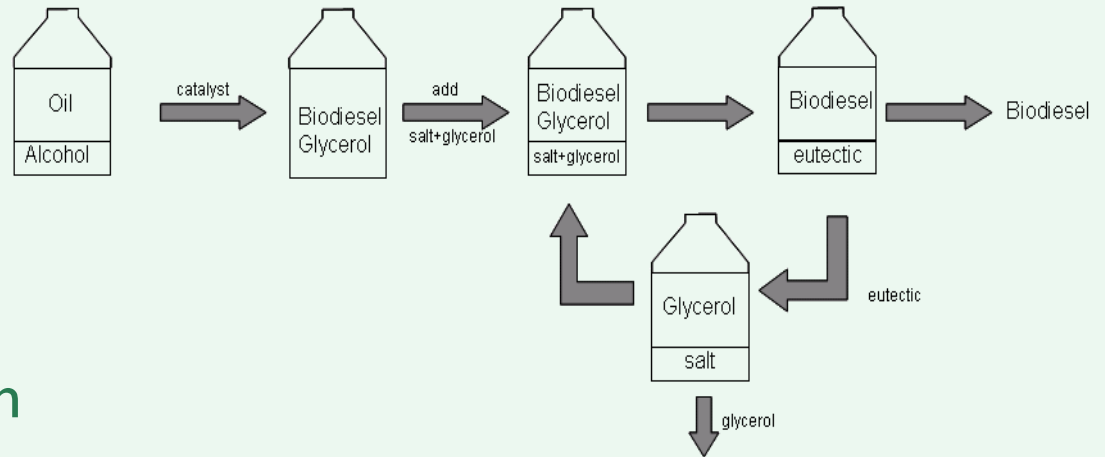
- Colloidal particles decrease viscosity
- Increase free volume



Electric Arc Furnace Dust

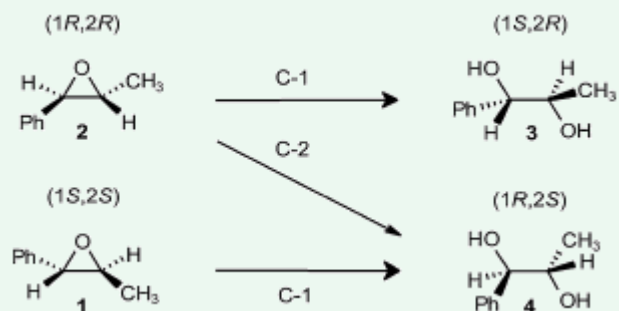


Dust contains 38% Fe, 33% Zn, 4% Pb and 1% Cd



Other applications

- Biodiesel purification
- Cleaning – Hard surface cleaners, surfactant delivery systems, antifungal/antimicrobial action, wipe delivery systems.
- Modification of cellulose with anionic/ cation functionalities
- Batteries – rechargeable zinc cells
- Antistatics, refractive index matches

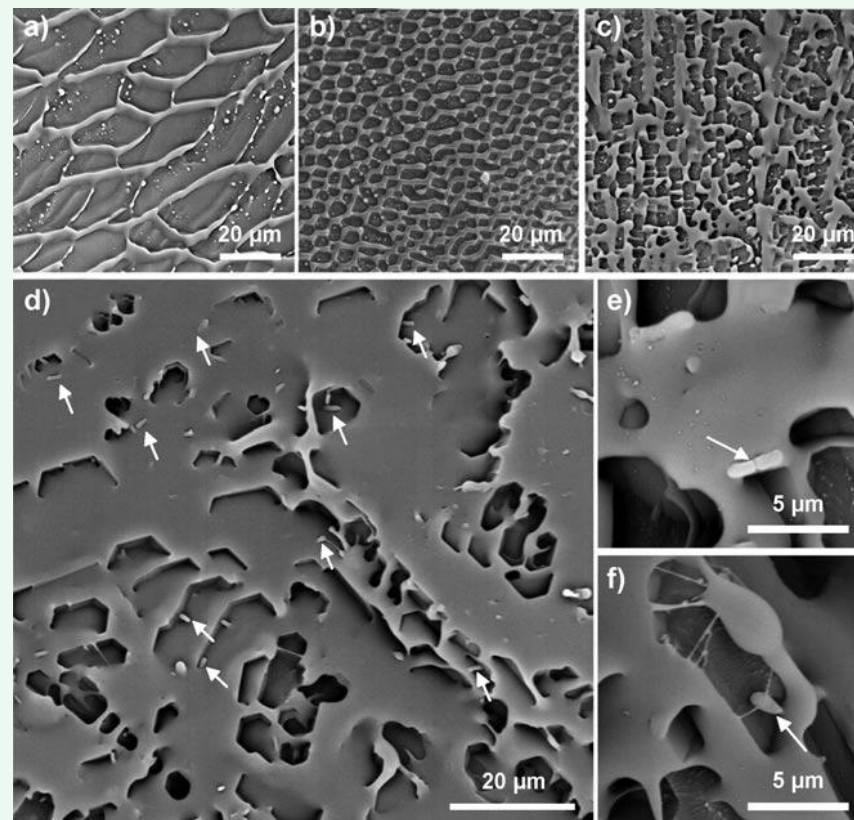


potato epoxide hydrolase StEH1
DESs improve product yield and
product distribution. Used as
mixtures with co-solvents.

Table 2
Steady state kinetic parameters for StEH1 catalyzed hydrolysis of (1S,1S)-2-MeSO, at different DES concentrations^a.

Solvent	Conc. (%)	k_{cat} (s ⁻¹)	K_M (mM)	k_{cat}/K_M (s μM) ⁻¹
Buffer	–	63 ± 3	0.077 ± 0.01	0.82 ± 0.1
GLY	20	51 ± 2	0.12 ± 0.01	0.42 ± 0.05
	40	57 ± 5	0.25 ± 0.04	0.23 ± 0.04
	60	44 ± 5	0.53 ± 0.09	0.082 ± 0.02
ET	20	63 ± 2	0.24 ± 0.02	0.26 ± 0.03
	40	61 ± 6	0.49 ± 0.08	0.12 ± 0.02
	60	31 ± 6	1.2 ± 0.3	0.026 ± 0.008
REL	20	65 ± 4	0.36 ± 0.04	0.18 ± 0.02
	40	92 ± 10	1.5 ± 0.3	0.060 ± 0.01

Lindberg et al., *J. Biotech.* (2010), 147, 169

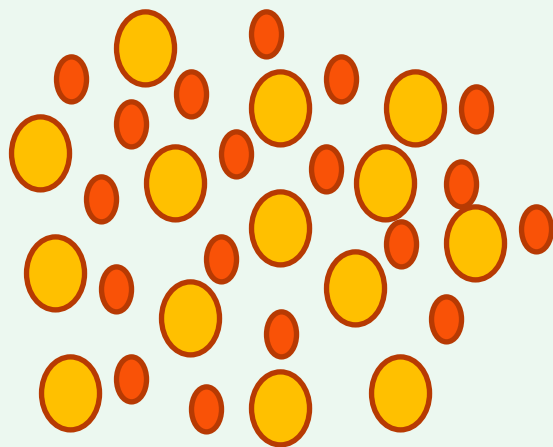


Tapping of E-coli bacteria in ChCl: glycerol

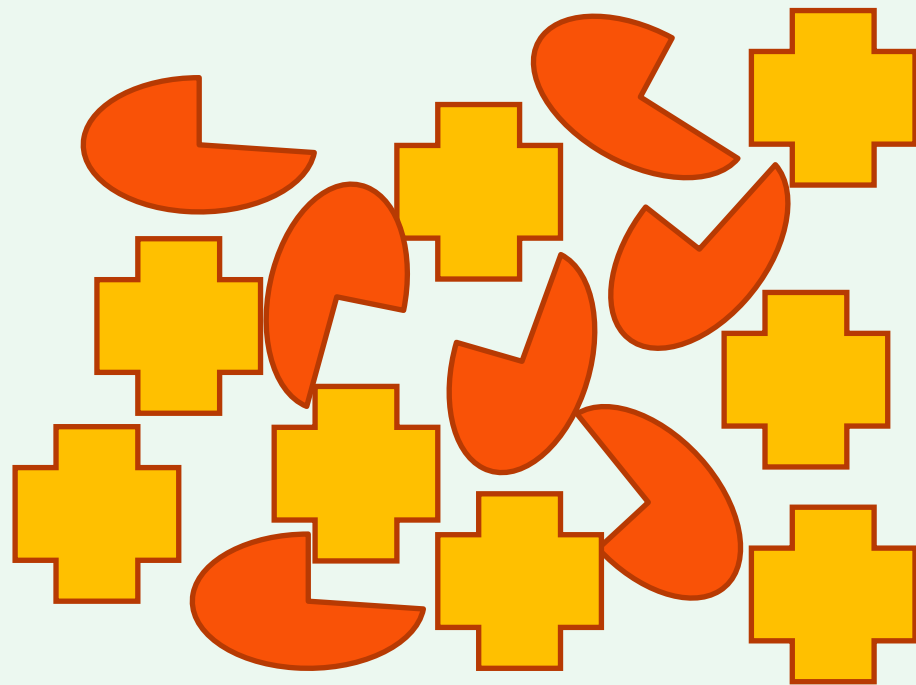
Gutierrez et al. *Angew. Chem., Int. Ed.*
(2010), 49, 2158

Molten salts vs. ionic liquids

- Ionic liquids are different from molten salts because of their ionic size and the temperature of the system.



Molten Salt



Ionic Liquid

Why are ionic liquids viscous?

- Because they have large ions and a small void volume



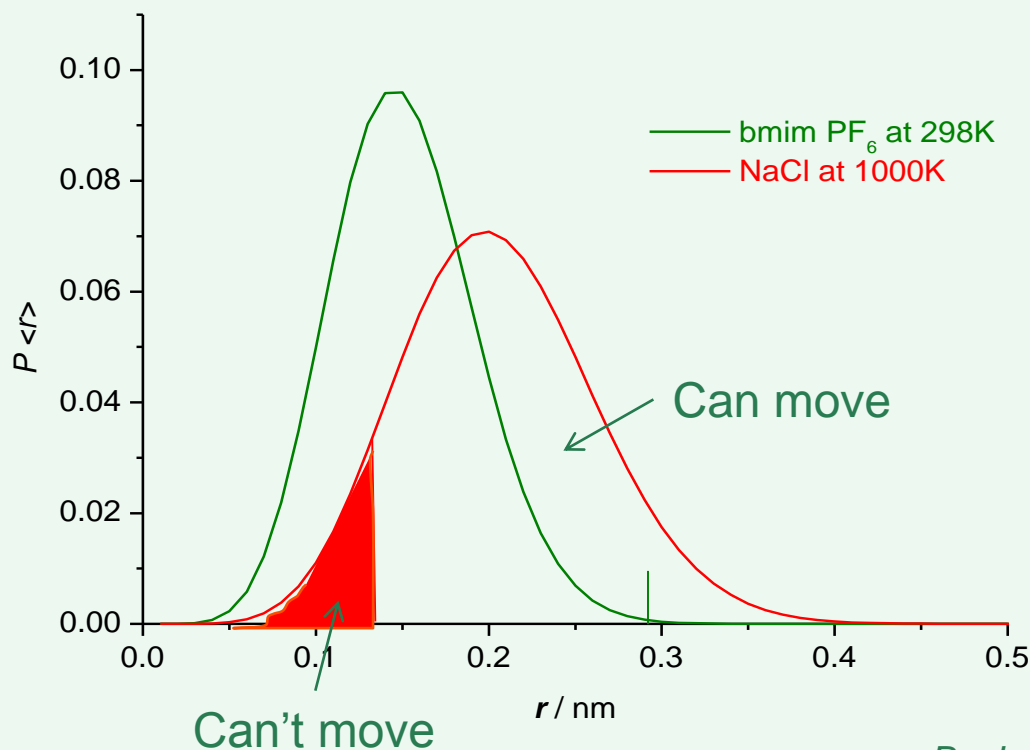
- Assume that an ionic liquid behaves like this slide puzzle – ions can only move if there are spaces next to them.

The model

The ions are large c.a. 0.4 nm

The holes are small c.a. 0.2 nm

One in a million ions has a hole next to it that is big enough to move into



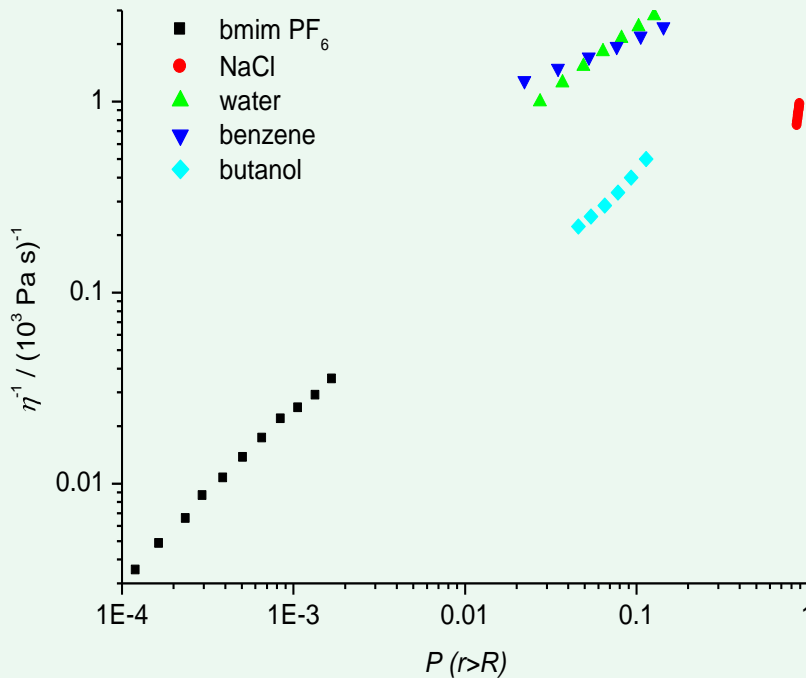
$$Pdr = \frac{16}{15\sqrt{\pi}} a^{7/2} r^6 e^{-ar^2} dr$$

hole size

$$a = 4\pi\gamma / kT$$

surface tension

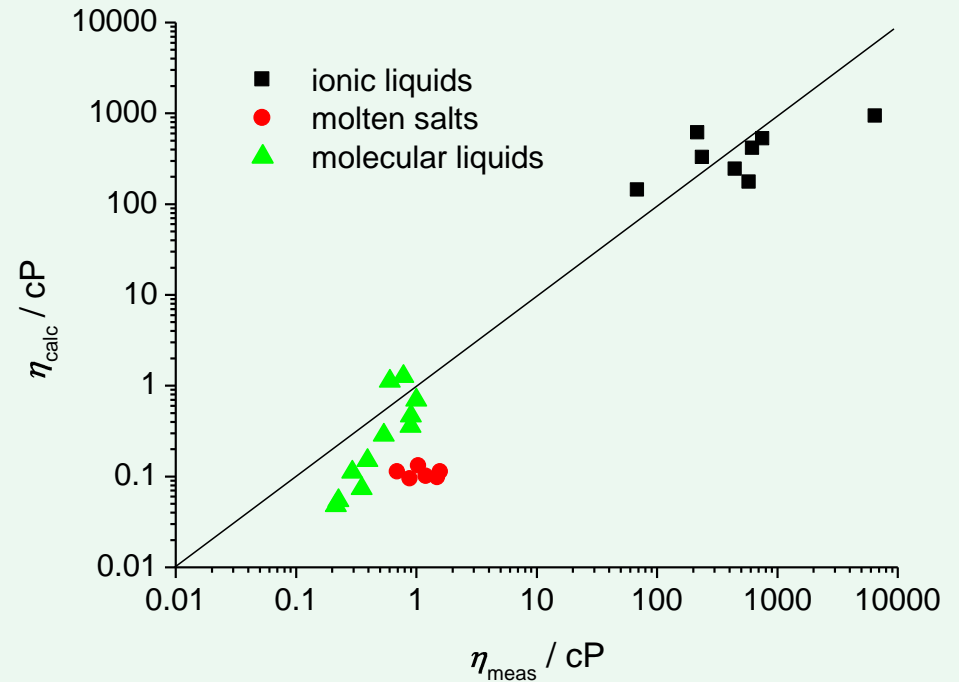
- Fluidity is proportional to hole probability



What is the constant of proportionality?

Hole Theory

If $P(r > R) = 1$ (ideal gas)

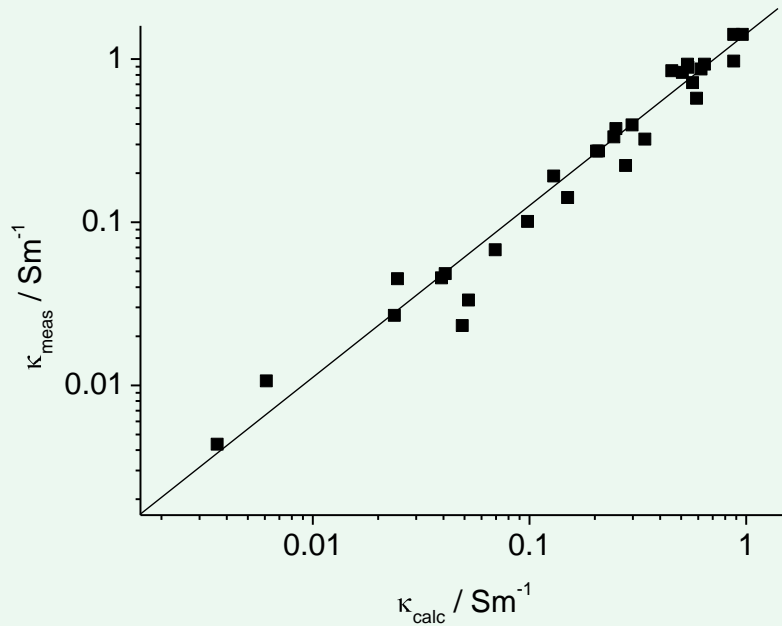
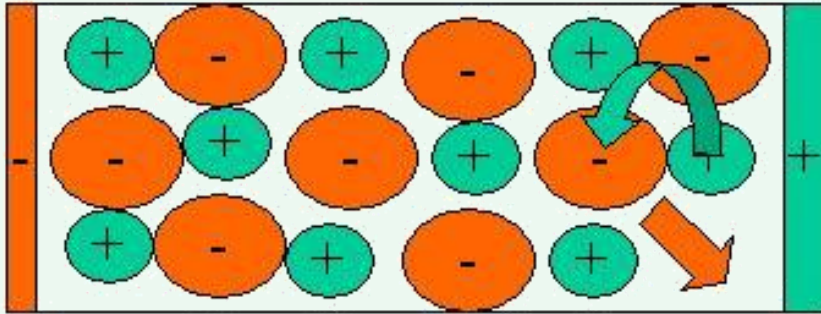


Viscosity mass speed area

$$\eta = \frac{m \bar{c} / 2.12 \sigma}{P(r > R)}$$

Limitation

- For molten salts the anion and cation have different sizes and therefore different transport numbers
- For ionic liquids transport numbers are more similar.



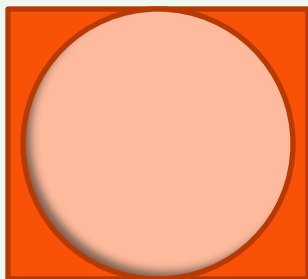
Conductivity – Hole Theory

- If hole concentration is very low hole migration must limit charge transport
- Hence conductivity is described by Nernst Einstein Equation
- $\lambda_+^o = z^2 F e / 6 \pi \eta R_+$
- Hence derive an equation for conductivity

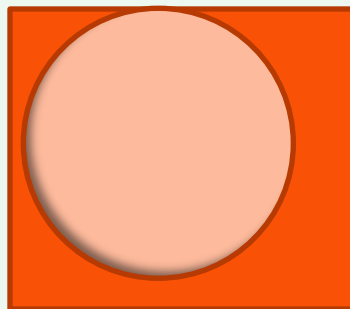
$$\kappa = \frac{z^2 F e}{6 \pi \eta} \left(\frac{1}{R_+} + \frac{1}{R_-} \right) \frac{\rho}{M_w}$$

Limitations

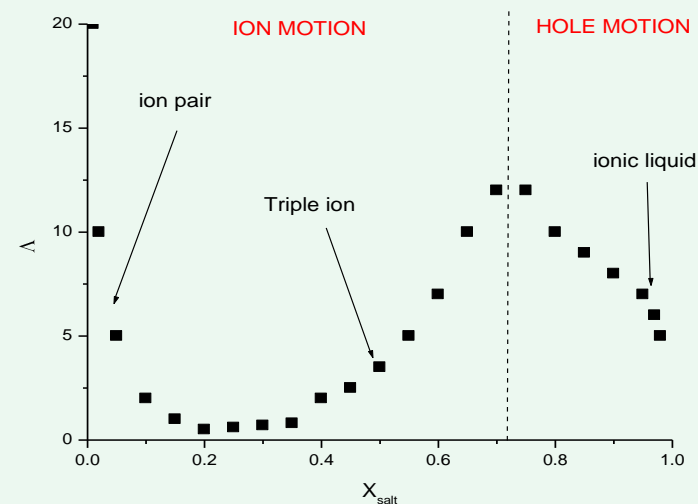
- Most cations are definitely not spherical
- The model is flawed because the ion does not need a similar sized hole to move into – It is the hole that moves.



Ion cannot move



Ion can move



Conclusions

- Ionic liquids based on choline chloride are useful for large-scale applications
- Versatile range of liquids possible
- Offer numerous social, environmental and economic advantages

Background Reading

- ❑ A. P. Abbott *Phys. Chem. Chem. Phys.* 2006, 8, 4265-4279
- ❑ A. P. Abbott, *Trans. I. M. F.* 86, 2008, 196-204
- ❑ F. Endres, A. P. Abbott and D. MacFarlane, *Electrodeposition using Ionic Liquids*, Wiley VCH, Weinheim, 2008

More information from

- ❑ www.ionmet.eu
- ❑ www.scionix.co.uk
- ❑ www.leicester-ils.co.uk/

